# DESIGN OF ANAEROBIC DIGESTION PROCESS FOR THE TREATMENT OF FIVE TONS PER DAY OF PETROLEUM SLUDGE

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***ABSTRACT***

*Untreated petroleum sludge constitutes health hazard to personnel on exposure and environmental hazard on disposal. The treatment of sludge destroys disease pathogens present in the sludge. Under microbial substrate limiting Mesophilic anaerobic digestion, a bioreactor for the treatment of 5 tons per day of sludge was designed. Dimensions of the bioreactor were obtained by substituting kinetic and experimental data into design equations. The potential of anaerobic digestion for the treatment of sludge was proved by a reduction in Biological Carbonaceous Oxygen Demand (BCOD) of the sludge from 6,080 mg/L to 20.40 mg/L and Total Hydrocarbon Content (THC) from 57,000 ppm to 1500 ppm. Gas Chromatography and Mass Spectrophotometry (GC-MS) result showed a decrease in concentration of priority Polycyclic Aromatic Hydrocarbons (PAHs) from thirties to units. Anaerobic digestion of 200 grams of sludge gave 10,500 $m^3$ /d biogas meaning 1 gram of sludge could yield 840 $m^3$ biogas for solids retention time of 16 days. The 183.50 $m^3$ Volume; 15.93 m height; 3.83 m diameter bioreactor design provided could help Nigerian industries and environmental agencies construct and install bioreactors for the treatment of their sludge at affordable cost. This will enhance Nigerian content in bioreactor manufacture and operation. With a bioreactor anaerobic digestion plant as a process unit in every Nigerian Process industry and Waste Water Treatment Plant, the problem of sludge treatment and disposal according to Environmental Protection Agency (EPA) standards and regulations will be solved.*

***Keywords:*** *Bioreactor, Petroleum Sludge; Priority toxicants; Anaerobic Digestion; Biochemical Carbonaceous Oxygen Demand; Total Hydrocarbon Content.*

## 1.0. INTRODUCTION

In Anaerobic digestion process, biodegradable material e.g. Sludge is broken down in a bioreactor in the absence of oxygen. Although the process involves a series of stages made of equipments; the major equipment in an Anaerobic digestion process is the bioreactor, where biological conversion processes occur. The limitation of this study is that the major equipment designed is the bioreactor. Petroleum industries generate large quantities of sludge which is a major source of environmental pollution (Islam, 2015). Petroleum sludge constitutes health hazard to personnel on exposure and environmental hazard on disposal, if not properly treated before disposal. Besides this, it is an economic waste to dispose sludge without treatment as the treatment yields important products such as biogas, pharmaceuticals, fertilizers, etc. (Appels *at al.*,2008). In this study, a Fed-batch bioreactor for the treatment of petroleum sludge is designed so as to make the sludge nontoxic to personnel on exposure, harmless to the environment on disposal. Islam (2015) states that petroleum sludges are hazardous wastes according to Environmental Protection Act and Hazardous Waste Handling Rules. These sludges cannot be disposed of as landfills even if they are de-oiled unless they are totally remediated. These sludges have to be treated and made harmless before disposal. Nigerian industries find it difficult to adhere to Environmental Protection Agency (EPA) Standards and Regulations for the treatment and disposal of sludge because they do not have bioreactors as an essential process unit in their process industries and waste water treatment plants. This is evidenced by numerous visits to most process industries where sludges are heaped with the hope of incinerating them in a burn pit. In Nigeria, hazardous wastes (sludge) have been dumped in various places e.g. Abattoir in Rivers State. The Nigerian government is recently embarking on clean up of areas polluted with sludge e.g. Ogoni land in Rivers State. In Nigeria, the treatment and disposal of sludge imposes a major challenge to the oil and gas industry. This study has provided a solution to this problem as the relevant industries and environmental agencies can now make use of the design data to fabricate and install suitable bioreactors for the treatment of their sludge at affordable cost. The treatment of sludge in bioreactors will eliminate the odour, health and environmental hazard associated with disposal of untreated sludge. Moreover, biogas a substitute for natural gas will be produced. This will enhance the realization of the Nigerian quest for self sufficiency in renewable energy. This is not a mere speculation as biogas sources are not yet fully utilized in Nigeria as it is in the advanced countries (Emberga *et al*., 2014; Osai, 2012; Fasina & Simonyan, 2013; Temilade, 2008). Kavitha & Pharm (2006) state that continuous stirred tank bioreactors are constructed according to recognized standards as published by International Standards Organization and British Standards Institute. These dimensions take into account both mixing, effectiveness and structural consideration. A mechanically stirred tank bioreactor is filled with a rushton turbine type impeller.

**Fig.1: Pictorial view of a Bioreactor**
**Source: Wikipedia (2014)**

Rao (2010) gives a generalized model for a Fed-batch bioreactor as in equation (1)

$$\frac{dC_i}{dt} = \frac{V(t)}{V_{Rc}}\left(C_{i,o} - C_i\right) + r_{fi} \quad (1)$$

Green & Perry (1997) state that the sludge is first hydrolysed to become water soluble and then degraded to produce volatile organic acids primarily acetic acid and hydrogen. *Methanogenic* bacteria then split the acetic acid to methane and carbondioxide (biogas). Impurities in the biogas are removed by pressure swing adsorption (PSA) on activated carbon. Since adsorption takes place at high temperature and pressure, desorption is achieved by depressurizing. Moisture is removed from the biogas by drying. The active site of the adsorbent retains water vapour and other pollutants thus decreasing adsorbent life, hence desorption is frequently carried out by depressurizing. Moreover, siloxanes are difficult to desorb from the adsorbent beds, so the adsorbent beds should be replaced regularly e.g. weekly. The biogas is dried, compressed and sent to storage.

Technical & Regulatory Guideline (2006) state that *methanogenic* bacteria prefer a relatively neutral pH of 6.6 to 7.4 and not acidic conditions. If acid formation is excessive the activity of the *Methanogenic* bacteria can be inhibited.

It is good practice to destroy the volatile acids as quickly as they are produced otherwise the volatile acids build up and depress the pH and eventually inhibit the *methanogenic* bacteria. To prevent this occurrence feed to the digester should be as uniform as possible and at short intervals as possible.

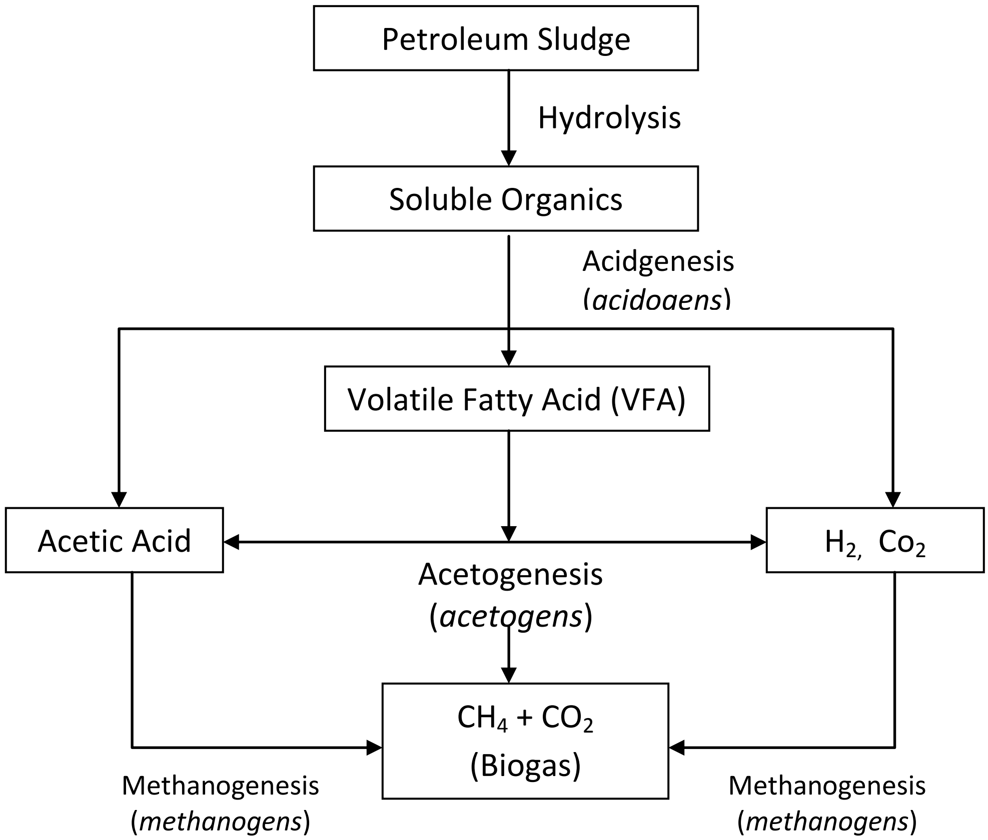


**Fig.2: Steps in anaerobic digestion process of Petroleum sludge**
**Source: Appels *et al*. (2008)**

Appels *et al.* (2008) give the steps to sludge biodegradability as follows: Hydrolysis, Acidogenesis, Acetogenesis and Methanogenesis among this, Hydrolysis is the rate limiting step. This rate limiting hydrolysis is enhanced by biological, chemical and mechanical interventions to the sludge. These interventions result in lysis or disintegration of sludge cells hence transforming the sludge into a biodegradable material. Hence, a test for the rate of biodegradability of sludge species, results in experimental data which fit into equations developed from kinetic models.

Anaerobic digestion results in the conversion of the biodegradable sludge to methane, carbon dioxide and microbial cells. Volatile suspended solids (VSS) produced are quite low. Biological carbonaceous oxygen demand (BCOD) is destroyed. Biogas produced range from 50 to 80 percent methane and 20 to 50 percent carbon (iv) oxide ($CO_2$) depending on the chemical characteristics of the sludge digested. The biogas produced is important for heat and power generation.

The pH should be maintained at 6.5 - 7.5 with the help of hydrochloric acid to avoid free ammonia toxicity. The use of nitric or sulphuric acid could result in significant operational problems.

**Process Description of the Bioreactor process**

Submerged immobilised *Methanogenic methanobrevibacter* bacteria acts on Petroleum sludge of pH 6.5 for a solids retention time of 16 days in fed-batch anaerobic bioreactor. The bioreactor is operated under substrate limiting mesphilic (37 $^{0}$C) anaerobic microbial digestion with the help of a vacuum pump which sucks air to maintain anaerobic condition. Nitrogen blaketting helps avoid reaction with oxygen.

The pH of 6.5 help avoid free ammonia toxicity which might inhibit the activity of the *methanogenic* bacteria. Higher temperatures (50-70 $^{0}$C) might be used if the process condition is thermophilic.

The biogas produced is sent to storage outside the battery limit of the plant with the help of a centrifugal compressor which help increase the pressure of the gas from 1bar to 5 bars to enhance transportation to storage. The biosolids produced from the anaerobic digestion of the sludge are dried in a rotary dryer and then pelletised in a pelletiser. The biosolids are useful as fertilizer and as soil conditioner. The biogas produced is useful for electrical power generation and heating and hence a substitute for natural gas.

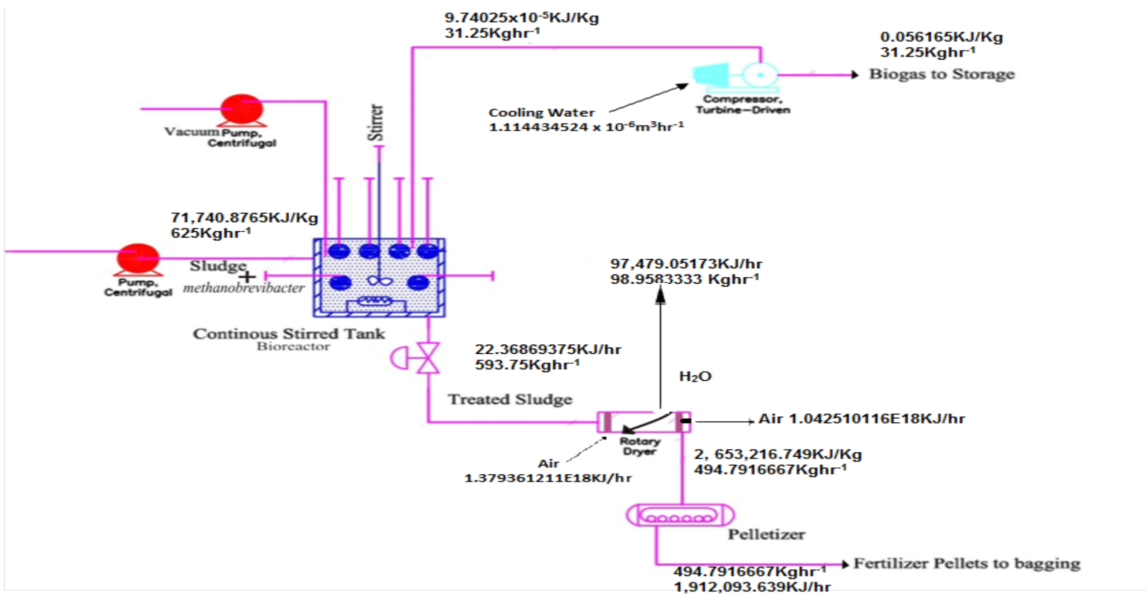


**Fig.3: Process- flow diagram for a Bioreactor Process**

## 2.0. MATERIALS AND METHODS

### 2.1. Materials

The following materials were used for the study:
Dissolved oxygen reagent bottles, Mineral water, 25ml density bottle, Hanna pH meter H196107, Muffle furnace LMF4, Thermospectronic spectrophotometer 4001/4, Oven, Gallenkamp incubator, Autoclave, Labtech anaerobic jar, Olympus microscope, Agilent gas chromatography and mass spectrophotometer (GC-MS) 7890 B, Spectr AA 55 B atomic absorption spectrophotometer, Petroleum sludge collected from a typical Petroluem Industry in Port Harcourt, Nigeria. *Methanogenic* Bacteria *(Methanobrevibacter)* isolated from the intestine of cow. OxoidAnaero Gen TM AN 0035A gas Park used in labtech anaerobic Jar to create anaerobic condition, Winkler reagent A & B.

### 2.2. Methods

200 grams of the sludge was measured using a chemical balance and put into a beaker. 2 grams of *methanogenic methanobrevibacter* bacteria was pip petted and put into the sludge in the beaker after which the beaker was put into labtech anaerobic jar with improvise for gas collection point. Anaerobic condition was maintained with the help of oxoid Anaerobic Gen TM AN 0035A gas park and catalyst. The anaerobic jar was corked airtight and kept in a Gallenkamp incubator maintained at 37 $^{0}$C (mesophilic) for a solids retention time of sixteen days. After performing a ten fold serial dilution; the Total Anaerobic Bacterial Count in cfu/g was calculated using the equation (2)

$$TABC = \frac{1}{DF} \times Average\ of\ plate\ bacterial\ count \times \frac{\mathbf{1}}{\mathbf{Volume\ Correction\ factor}} \quad (\mathbf{2})$$

The percent Volatile Suspended Solids (VSS) measured using gravimetric method was calculated using equation (3)

$$Volatile\ Suspended\ solids = \frac{Weight\ of\ Volatile\ residue}{Weight\ of residue} \times \frac{100}{1} \qquad (3)$$

The Total Hydrocarbon Content (THC) measured using spectrophotometric method was calculated using equation (4)

$$THC = \frac{Absorbance\ of\ sludge \times Gradient\ of\ standard\ graph}{weight\ of\ sample\ diluted\ in\ 100ml \times \frac{1}{Dilution\ Factor}} \qquad (4)$$

The Biochemical Carbonaceous Oxygen Demand (BCOD) measured using the Winkler's method was calculated using the equation (5)

$$BCOD_5 = \frac{DO_{initial} - DO_{Final}}{DilutionFactor} \qquad (5)$$

The concentration of Polycyclic Aromatic Hydrocarbons (PAHs) in the sludge and in the biosolids produced from anaerobic digestion of the sludge was measured using Gas Chromatography – Mass Spectrophometry (GC-MS).

### 2.2.1. Kinetic Models

The following kinetic models were derived in Sampson (2016).

**For the Biomass**

$$\frac{dX_1}{dt} = D\left(X_{1,0} - X_1\right) + \frac{\mu m X_1 X_2}{k_m + X_2} \quad (6)$$

**For the Sludge**

$$\frac{dX_2}{dt} = D\left(X_{2,0} - X_2\right) - \frac{\mu_m X_1 X_2}{Y(k_m + X_2)} \quad (7)$$

Comparing it with equation (1)

$$\frac{dC_i}{dt} = \frac{V_t}{V_{RC}}\left(C_{i,0} - C_i\right) + r_{fi}$$

Dilution rate = $V_t / V_{RC} = D$

**For Biomass:**

$$r_{fi} = +\frac{\mu_m X_1 X_2}{K_m + X_2} - k_d X_1 \quad (8)$$

The positive sign depicts that the biomass is multiplying.

**For Sludge:**

$$r_{fi} = -\frac{\mu_m X_1 X_2}{\gamma(K_m + X_2)} \quad (9)$$

This gives the rate of reaction. The negative sign depicts that the sludge is biodegrading. Note that $K_d X_1$ is not included in the $r_{fi}$ for sludge because $K_d$, the endogenous respiration coefficient is zero for the sludge. $\frac{dx_2}{dt} = \frac{\mu_m x_1 x_2}{Y(km + x_2)}$ gives the rate of reaction $rf_i$. Therefore equation (1) can be written in another form as:

$$\frac{dX_2}{dt} = D\left(X_{2,0} - X_2\right) - \frac{\mu_m X_1 X_2}{\gamma(K_m + X_2)}$$

### 2.2.2. Design Equations

Equation (10) was derived for volume of the bioreactor.

Levenspiel (2001) give rate of reaction as

$$-r_A \quad = KC_A$$

But $C_A = C_{A_O} (1 - X_A$

$$-r_A \quad = KC_{A_O} \ (1 - X_A)$$

Substitute this for $-r_A$ in the equation obtained from Levenspiel (2001)

$$V_R = \frac{NA_o}{t} \int_O^{XA} \frac{dX_A}{(-r_A \quad)}$$

$$V_R = \frac{NA_o}{t} \int_O^{XA} \frac{dX_A}{KCA_o \, (1 - X_A \quad)}$$

$$V_R = \frac{NA_o}{tKCA_o} \int_O^{XA} \frac{dX_A}{(1 - X_A \quad)}$$

Substituting $K_m$ for K, $X_{2,0}$ for $C_{A_O}$ and considering the fractional change in volume

$$V_R = \frac{NA_o}{tK_m X_{2,0}} \int_O^{XA} \frac{dX_A}{(1 - X_A)(1 + E_A X_A)} \qquad (10)$$

Where $V_R$ is the volume of the Bioreactor

$$\text{Yield Coefficient (Y)} = \frac{mgVSS}{mg\ BCOD} \qquad (11)$$

Appels *et al*. (2008) give equation for Net mass of cell tissue produced per day:

$$P_x = \frac{YES_0}{1 + k_d \theta_c} \qquad (12)$$

Volume of Biogas produced was calculated using equation

$$V_{CH4} = (0.35)(S_0 - s)(Q)\left(\frac{10^3 g}{(kg)^{-1}}\right) - \quad 1.42P_x \qquad (13)$$

Tapobrata (2011) give the following equations for bioreactor fundamental dimensions:

**Height of Bioreactor**

$$h = \frac{4V_R}{\pi D^2} \qquad (14)$$

**Impeller Diameter of Bioreactor**

$$\frac{D_i}{D} = 0.3$$

$$D_i = D \times 0.3 \qquad (15)$$

**Width of Baffle**

$$(0.08 - 0.1)D_i \quad (16)$$

**Length of Jacket**

$$J_L = \frac{1}{4}H \quad (17)$$

**Vertical Distance between adjacent stirrer blades**

$$\frac{I_L}{D_i} = 1.2 \quad (18)$$

$$\text{Poison ratio} = \frac{\text{hemispherical thickness}}{\text{Cylinder thickness}} \quad (19)$$

$$\textbf{Volume of hemisphere} = \frac{2}{3}\pi \times r^3 \div 2 \quad (20)$$

$$\textbf{Volume of conical bottom} = \frac{1}{8}V_R \quad (21)$$

$$\textbf{Height of conical bottom} = \frac{\frac{1}{8V_R} \times 3}{\pi r^2} \quad (22)$$

## 3.0. RESULTS

### 3.1. Data Obtained

**Table 1: Experimental Data Obtained**

| Parameter | Value |
|---|---|
| Initial concentration of Biomass $(X_{1,0})$ | 1.0 $mg/l$ |
| Initial concentration of sludge $(X_{2,0})$ | 0.3383 $mg/l$ |
| Volatile suspended solids (VSS) | 99.6 % |
| Biochemical carbonaceous oxygen demand (influent sludge) | 6080 $mg/L$ |
| Biochemical carbonaceous oxygen demand (effluent biosolids) | 20.40 mg/L |
| Yield coefficient $(Y)$ | 0.016 |
| Maximum specific growth rate $(\mu_m)$ | 0.0738 $hr^{-1}$ |
| Dilution rate $(D)$or space velocity | 0.18 $hr^{-1}$ |
| Total hydrocarbon content (influent sludge) | 57000 ppm |
| Total hydrocarbon content (effluent biosolids) | 1500 ppm |
| Negative of log of Hydrogen ion Concentration (pH) | 6.5 |
| Net mass of cell tissue produced per day | 62.5 kg/d |
| Volume of biogas produced | 10,500 $m^3$/d |
| Polycyclic aromatic hydrocarbons (influent sludge) | Thirties (mg/l) |
| Polycyclic aromatic hydrocarbons (effluent biosolids) | Units (mg/l) |
| Monods Constant $(K_m)$ | 0.02 $kmol/m^3$ |
| Endogenous respiration Coefficient $(K_d)$ | 0.025 $d^{-1}$ |
| Total Anaerobic Bacterial Count (TABC) | Day 1: 0.129 × $10^9$; Day 2: 102.1 × $10^7$; Day 5: 2020 × $10^9$; Day 16: 7.199 × $10^9$ (cfu/g) |

### 3.2. Sizing the Bioreactor

Quist (2007) give equation (23):

$$C_5H_7O_2N + 4H_2O \xrightarrow{Methanobrevibacter} 1.5CO_2 + 2.5CH_4 + NH_4^+ + HCO_3^-$$

Where $\varepsilon_A$ is given by

$$\Sigma CR: 1 + 4 = 5$$

$$\Sigma CP: 1.5 + 2.5 + 1 + 1 = 6$$

$$\varepsilon_A = \frac{\Sigma CP - \Sigma CR}{\Sigma CR} = \frac{6-5}{5}$$

$$\varepsilon_A = \frac{1}{5} = 0.2$$

Levenspiel (2001) give formula for conversion

$$X_A = 1 - \frac{CA}{CAo}$$

$$X_A = 1 - \frac{X_2}{X_{2,0}}$$

$$X_{2,0} = 0.3383 \text{ mg/l}$$

$$X_2 = 0.228893 \text{ mg/l}$$

Note that treatment of sludge is a slow reaction hence conversion must be low.

$$X_A = 1 - \frac{0.2289}{0.3383}$$

$$X_A = 1 - 0.6766$$

$$X_A = 0.3234$$

Coulson & Richardson (1991) give the Monods constant

Km : 0.02 mol/$m^3$

t: solids retention time, 16 days

$C_{Ao}$: initial concentration of sludge

$C_{Ao} = X_{2,0} = 0.3383$

$N_{Ao}$: Number of moles of sludge

Molar mass of $C_5H_7O_2N$: (12×5)+(1×7)+(16×2)+(14×1) = 60+7+32+14=113

**Plant Capacity**: Given a Plant capacity of 5 Tons per day. Knowing that 1Ton is equivalent to 1000 kg, So 5 Tons is equivalent to 5000 kg which is the mass of sludge digested per day.

$$= \frac{\text{Mass}}{\text{Molar Mass}} = \frac{5000\text{kg}}{113}$$

= 44.24778761 kmol/day

= 44.24778761×$10^3$ moles/day

= 44,247.78761 moles/day

Recall equation (10)

$$V_R = \frac{N_{AO}}{C_{AO}.\text{t.Km}} \int_0^{XA} \frac{d\,X_A}{(1 - xA)(1 + \varepsilon_A X_A)}$$

Substituting $X_{2,0}$ for $C_{A0}$ in eqn (38) $X_{2,0} = C_{A0}$

$$V_R = \frac{N_{Ao}}{X_{2,0} tKm} \int_0^{0.3234} \frac{dX_A}{(1 - XA)(1 + \varepsilon_A X_A)}$$

$$V_R = \frac{44{,}247.78761}{0.3383x16x0.02}\int_0^{0.3234}\frac{d\,(0.3234)}{(1-0.3234(1+0.2x(0.3234)}$$

$X_A = 0.3234$
$K_m = 0.02\ mol/m^3$
$C_{Ao} = 0.3383\ mg/L$
t = 16 days
$N_{Ao} = 44{,}247.78761$ moles/day
$\varepsilon_A = 0.2$
Using MATHCAD Software
$V_R = 1.835 \times 10^5$ Litres
(1000 liters = $1m^3$)

Therefore: $V_R = \frac{1.835\times10^5}{1000} = \frac{1,83500.00}{1000}$

= 183.50 $m^3$
Volume of Bioreactor = 183.50 $m^3$

### 3.3. Optimization

Coulson & Richardson (2009) give equation for purchased equipment cost.

$$PEC = a + b\ s^n\ \times MF \quad (24)$$

Where:
$PEC$ is the purchased equipment cost. $a$ & $b$, cost constants peculiar to the equipment.
$s$ ,the characteristics size parameter
$n$, the index characteristic of equipment size
Recall that:
$a = 28{,}000$ in 2010
That is, 28,000 mutiplied by 1.96 in 2018 is equal to 54,880
Range for $b$: 0 to 104,000
$s$ is same for 2018 as it was in 2010

$$s = 0.5$$

$n$ is same for 2018 as it was in 2010.

$$n = 0.8$$

MF, materials factor for stainless steel = 1.3 multiplied by 1.96 in 2018 is equal to 2.548
≈ 2.55 in 2018

**Table 2: Optimization of Bioreactor Diameter**

| Diameter D(m) | $a$ | $b$ | $s$ | $bs$ | $a+b$ | $a+bs$ | $n$ | $bs^n$ | $MF$ | $a+bs^n$ | Cost $a+bs^n\ MF$ |
|---|---|---|---|---|---|---|---|---|---|---|---|
| 0 | 0 | 0 | 0 | 0 | 0 | 0 | 0 | 0 | 0 | 0 | 0 |
| 0.5 | 6,875 | 12,985 | 0.5 | 6,492.5 | 19,860 | 13,367.50 | 0.8 | 1,121.84 | 2.55 | 7996.84 | 20,391.93308 |
| 1.0 | 13,750 | 25,970 | 05 | 12,985.0 | 39,720 | 26,735 | 0.8 | 1,953.23 | 2.55 | 15,703.23 | 40,043.23854 |
| 1.5 | 20,625 | 38,955 | 0.5 | 19,477.50 | 59,580 | 40,102.5 | 0.8 | 2,701.63 | 2.55 | 23,326.64 | 59,482.91762 |
| 2.0 | 27,500 | 51,940 | 0.5 | 25,970.0 | 79,440 | 53,470 | 0.8 | 3,400.77 | 2.55 | 30,900.77 | 78,796.96947 |
| 2.5 | 34,375 | 64,925 | 0.5 | 32,462.50 | 99,300 | 66,837.5 | 0.8 | 4,065.42 | 2.55 | 38,440.42 | 98,023.0746 |
| 3.0 | 41,250 | 77,910 | 0.5 | 38,955.0 | 119,160 | 80,205 | 0.8 | 4,703.82 | 2.55 | 45,953.82 | 117,182.2375 |
| 3.5 | 48,125 | 90,895 | 0.5 | 45,447.50 | 139,020 | 93,572.5 | 0.8 | 5,321,18 | 2.55 | 53,446.18 | 136,287.7605 |
| 4.0 | 55,000 | 103,880 | 0.5 | 51,940.0 | 158,880 | 106,940 | 0.8 | 5,921.09 | 2.55 | 60,921.09 | 155,348.7758 |

PEC for the bioreactor in the year 2018 gave *£ 148,906.4103.*
Interpolation for the Diameter of the Bioreactor at *£ 148,906.4103* gave 3.83 meters.

**Table 3: Bioreactor Fundamental Dimensions**

| Parameter | Value |
|---|---|
| Volume of the Bioreactor ($V\_R$ ) | 183.50 $m$^3 |
| Diameter of the Bioreactor ($D$) | 3.83 $m$ |
| Height of Bioreactor ($H$) | 15.93 $m$ |
| Impeller Diameter of Bioreactor ($D\_i$ ) | 1.149 $m$ |
| Width of Baffle ($W\_b$ ) | 11.49 $cm$ |
| Length of Jacket ($J\_L$ ) | 3.9825 $m$ |
| Vertical distance between adjacent stirrer blades ($I\_L$ ) | 1.3799 $m$ |
| Radius of Hemispherical head | 1.915 $m$ |
| Height of Hemispherical head | 1.0 $m$ |
| Radium of conical bottom | 1.915 $m$ |
| Height of conical bottom | 6.0 $m$ |

### 3.4. Design Features

#### 3.4.1. Material of Construction

Stainless steel.

#### 3.4.2. Wall Thickness

Coulson & Richardson (2009) give 14$mm$ as the minimum thickness for a vessel of diameter 3.5$mm$ – 4.0$mm$.
Wall thickness of bioreactor = 14 $mm$.

#### 3.4.3. Vessel Pressure

Coulson & Richardson (2009) give a pressure of 1 bar for vessels operated anaerobically. Pressure = 1 bar.

#### 3.4.4. Spacing between the jacket and vessel wall

The spacing between the Jacket and vessel wall is 50 mm (Coulson & Richardson, 2009).

#### 3.4.5. Thickness of Jacket

Thickness of Jacket or lagging is 50 mm.
**3.4.6. Lagging Material:** Foam glass (Cellular glass made by fusing powered glass with Carbon particles.)

**3.4.7. Cover for Lagging:** Aluminum metal sheet (0.5 mm thick).
**3.4.8. Support:** Concrete pillars.
**3.4.9. Stirrer Driver:** Rushton turbine.

### 3.4.10. Hemispherical Head

#### 3.4.10.1. Radius of hemispherical head

Radius of cylinder = 1.915 meters, and equal to the radius of hemispherical head.

#### 3.4.10.2. Height of Hemispherical head

Take volume of hemisphere to be $\frac{1}{3}$ volume of cylinder.

Volume of hemisphere (half of a sphere) $= 2/3 \times \pi \times r^\wedge 3 \div 2$

Radius of the hemisphere $= 1.915\ metres$

Therefore:

Height of the hemisphere $= \frac{1.915}{2} = 0.9575 \approx 1.0\ metres$

### 3.5. Conical Bottom

#### 3.5.1. Radius of conical bottom

Radius of Conical Bottom is same as radius of cylinder $= 1.915\ metres$.

Volume of the conical bottom is one eight the volume of the cylinder.

Volume of cylinder $= 183.50\ m^\wedge 3$

### 3.6. Height of Conical Bottom

Volume of the conical bottom is one eighth the volume of the cylinder.

Volume of cylinder $= 183.50\ m^\wedge 3$

Volume of conical bottom: $\frac{1}{8} \times 183.50\ m^3 = 22.9375\ m^3$

$$= 1/3\ \pi r^\wedge 2\ h \qquad (25)$$

$$22.9375 = \frac{1}{3} \times 3.142(1.915)^2 h \approx 6.0\ metre$$

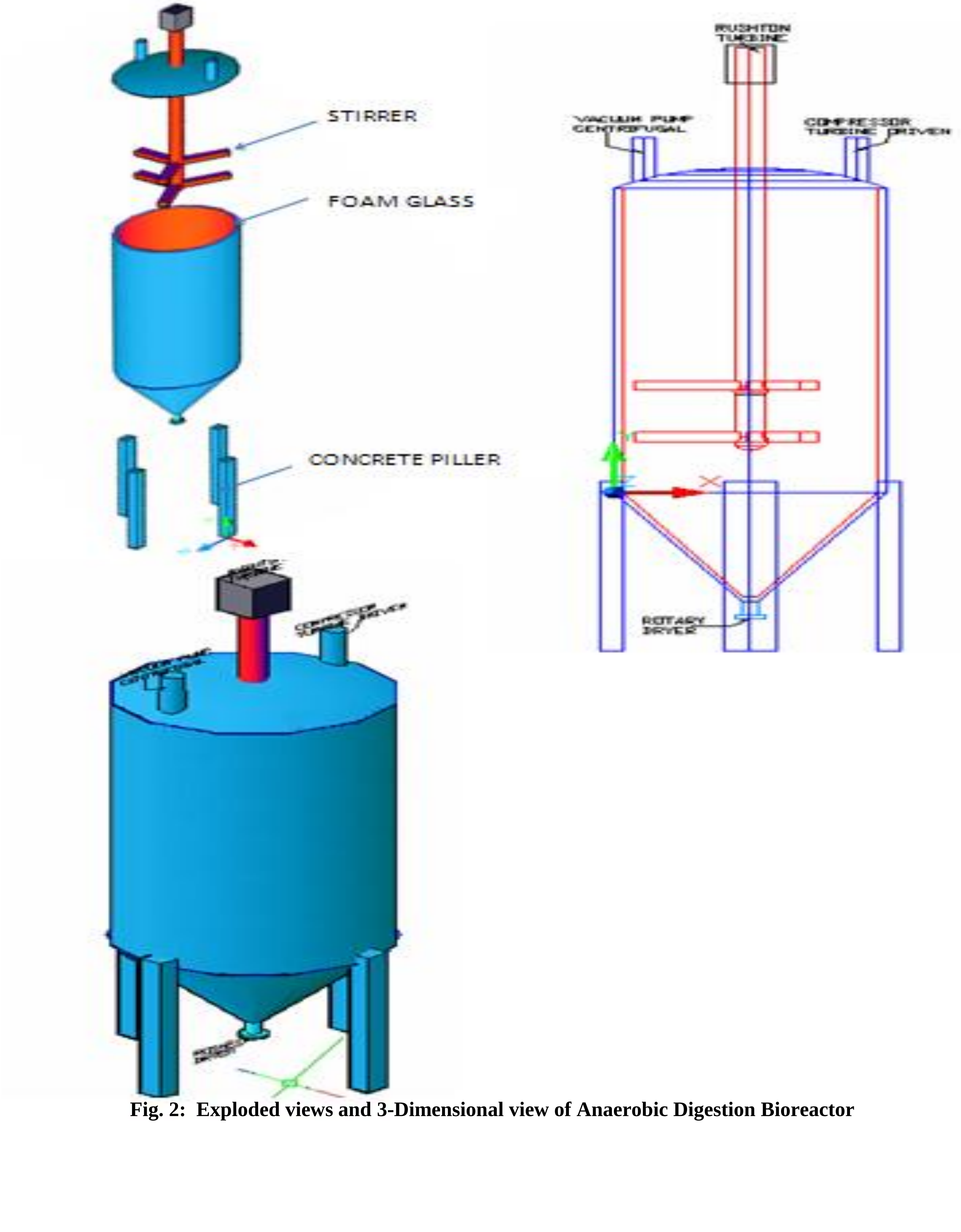


**Fig. 2: Exploded views and 3-Dimensional view of Anaerobic Digestion Bioreactor**

## 4.0. DISCUSSION

The result of the TABC indicates that micro-organisms multiplied in the biological reaction. The microbial digestion was terminated after 16 days at the falling rate phase when most of the micro-organisms must have died. BCOD and THC decrease with sludge biodegradation. BCOD and THC can therefore be used as a measure of sludge biodegration. The concentration of Napthalene, Anthracene and phenanthrene in the untreated sludge reduced from Thirties to Units after the sludge treatment. According to Owabor & Owhiri (2011), Napthalene, Phenanthrene and Anthracene are used as representative of the polycyclic aromatic hydrocarbons as they are in the priority toxicant list of EU and USEPA due to their Mutagenic and carcinogenic properties.

A reasonable volume of biogas can be produced in substantial amount from anaerobic digestion of the sludge as shown in analysis of equation (13). 200 g sludge yielded 10,500 $m^3$/d biogas for 16 days. Considering 200 days operation per year. 1g sludge would yield 10,500/200=52.5 $m^3$/d biogas for 16 days.52.5×16 = 840 $m^3$ biogas from 1g of sludge.

A bioreactor of volume 183.50 $m^3$, diameter 3.83metres and height 15.93 metres can be constructed as shown in figure 2. However, the bioreactor can be scaled-up or scaled-down or remodified to meet the needs of an industry or agency.

Stainless steel is used as material for construction because it does not get easily corroded. Spacing between jacket and vessel wall must be high enough to enhance insulation. Lagging must be thick enough to enhance heat conservation. Foam glass is chosen as lagging material because it is dense enough to allow for attachment of fittings and sealing and does not absorb moisture. Aluminum metal sheet is chosen as cover for lagging because it is cheap enough and is non corrosive. Concrete pillars are chosen as support because they cannot conduct electricity. Rushton turbine is chosen as stirrer driver because it is more robust and has higher efficiency than electrical motors.

A hemispherical head is the strongest shape, capable of resisting about twice the pressure of a torispherical head of the same thickness (Coulson & Richardson, 2009). Conical bottom is used to facilitate the smooth flow and removal of solids from a process equipment (Coulson & Richardson, 2009).

## 5.0. CONCLUSION

A bioreactor with the following fundamental dimensions: Volume 183.50 $m^3$; diameter 3.83 metres; height 15.93 metres has been designed. Other dimensions of the designed bioreactor are: impeller diameter 1.149 metres; width of baffle 11.49 cm; length of jacket 3.9825 metres; vertical distance between adjacent stirrer blades 1.3788 metres; wall thickness 14 mm; spacing between jacket and vessel wall 50 mm; thickness of jacket 50mm; Radius of hemispherical head 1.915 metres; Height of hemispherical head 1.0 metre; Radius of conical bottom 1.915 metres; Height of conical bottom 6.0 metres. With this design, the problem of sludge treatment in accordance with EPA standards and regulations for the treatment and disposal of sludge has been solved. The relevant industries and environmental agencies can now fabricate and install bioreactors for the treatment of their sludge at affordable cost. This could enhance Nigerian content in Bioreactor manufacture and operation. The potential of anaerobic digestion for the treatment of petroleum sludge has been proved by a decrease in the concentration of polycyclic aromatic hydrocarbons. The priority toxicants in the sludge (Naphthalene, Phenanthrene and anthracene) decreased in concentration from thirties to units. The biochemical carbonaceous oxygen demand decreased from $6080\ mg/l$ to $20.40\ mg/l$ and the total hydrocarbon content of the sludge from 57000 ppm to 1500 ppm. Hence anaerobic digestion helps to transform the toxic petroleum sludge to harmless biosolids. It was found that the treatment of 5 Tons per day of petroleum sludge could yield *10,500* $m^3$ per day of biogas; hence, one gram of the sludge could yield $840m^3$ biogas for a solid retention time of sixteen days. Biogas, being a renewable energy source and a better substitute for natural gas, anaerobic digestion of petroleum sludge could enhance the realization of the Nigeria quest for self sufficiency in sustainable energy. The plant should be located as a process unit in every Nigerian process industry, waste water treatment plants and sites where sludge is dumped.

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# APPENDIX

## 7.0. NOMENCLATURE

| Symbol | Definition | Unit |
|---|---|---|
| **$C_i$** | Inlet concentration of component i | $kmol/m^3$ |
| **$C_{i,o}$** | Initial concentration of component i | $kmol/m^3$ |
| **$D_i$** | Impeller diameter | m |
| **E** | Efficiency of sludge utilization | % |
| **$F_{AO}$** | Molar Feed rate | $mols^{-1}$ |
| **H** | Height of the Bioreactor | m |
| **$I_L$** | Vertical distance between adjacent stirrer blades | m |
| **$J_L$** | Length of the jacket | |
| ***K_m*** | Monods constant | $kmol/m^3$ |
| ***k_d*** | Endogenous respiration coefficient or specific maintenance rate | $(d^{\wedge}(-1))$ |
| **m** | Mass of dry solids | kg |
| **$N_{A0}$** | Number of moles | mols/day |
| **$P_s$** | Percent solids expressed as decimal | |
| ***P_x*** | Net mass of cell tissue produced per day | $kg/d$ |
| **Q** | Flow rate of methane Number | $m^{\wedge}3 / d$ |
| **R** | Gas constant, | kJ/kmol K |
| **$r_{fi}$** | Rate of reaction of component i | $mgl^{-1}s^{-1}$ |
| **S** | Biological carbonaceous oxygen demand (BCOD) in the effluent biosolids | $mg/l$ |
| **$S_D$** | Side depth of Bioreactor | m |
| ***S*_0** | Biological carbonaceous oxygen demand (BCOD) in the influent Sludge | $mg/l$ |
| **t** | Time | days |
| **$V_R$** | Volume of Bioreactor | $m^3$ |
| **$V_{RC}$** | Culture Volume | $m^3$ |

| | | |
|---|---|---|
| **V(t)** | Volumetric Feed rate at time t | $m^3/d$ |
| $V_{CH_4}$ | Volume of methane produced | $m^3/d$ |
| $X_A$ | Conversion | |
| $X_1$ | Biomas conentration | mg/l |
| $X_{1,0}$ | Initial concentration of biomass | mg/l |
| $X_2$ | Sludge conentration | mg/l |
| $X_{2,0}$ | Initial concentration of Sludge | mg/l |
| **Y** | Yield coefficient given as mass of sludge or biomass produced per unit biosolids removed | |
| **Ƶ** | Depth of bed | m |
| $\theta_c$ | Mean cell residence time | days |
| $\mu_m$ | Maximum specific growth rate or half minimal velocity concentration | $hr^{-1}$ |
| $\rho$ | Density | $kg/m^3$ |
| $\rho_w$ | Specific weight of water | $kg/m^3$ |

## Abbreviations

| **Abbreviation** | **Definition** |
|---|---|
| BCOD | Biological Carbonaceous Oxygen Demand |
| DF | Dilution Factor. |
| DO | Dissolved Oxygen |
| EPA | Environmental Protection Agency |
| EU | European Union |
| FAO | Food and Agricultural Organization |
| GC – MS | Gas Chromatography and Mass Spectrophotometry |
| MF | Materials Factor |
| PAHs | Polycyclic Aromatic Hydrocarbons |
| PEC | Purchased Equipment Cost |
| SRT | Solids Retention Time |
| TABC | Total Anaerobic Bacterial Count |
| THC | Total Hydrocarbon Content |
| USEPA | United States Environmental Protection Agency |
| VSS | Volatile Suspended Solids |
| WWTP | Waste Water Treatment Plant |